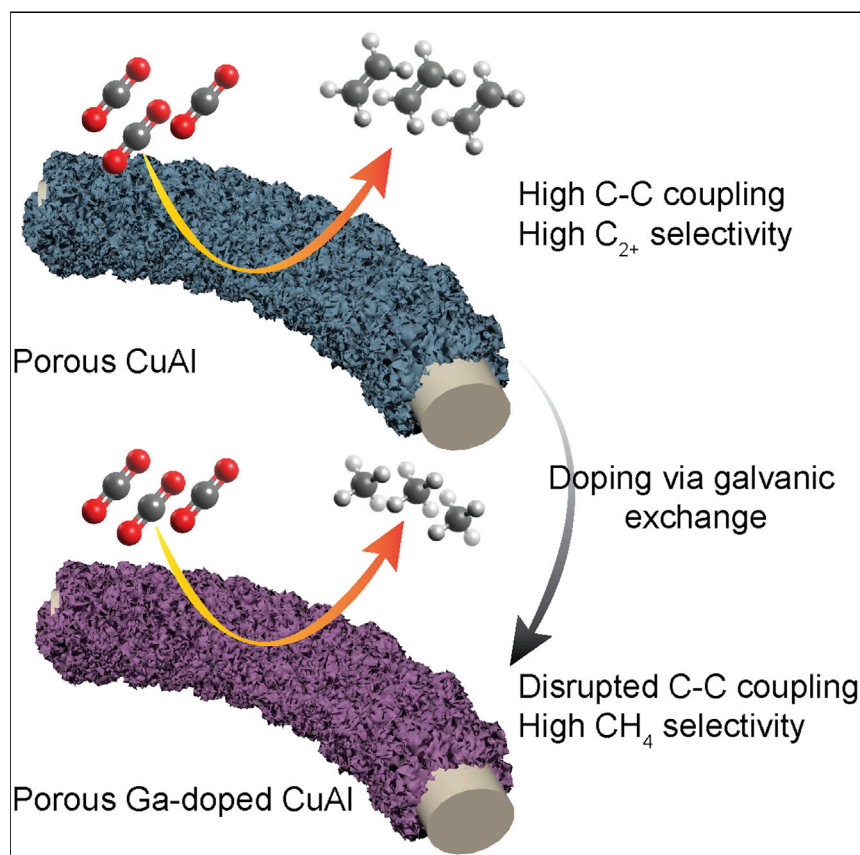


Article

Ga doping disrupts C-C coupling and promotes methane electroproduction on CuAl catalysts



We shift the CO_2 reduction reaction (CO_2RR) product distribution from C_{2+} products toward methane. Ga doping in CuAl catalysts disrupts carbon-carbon coupling and results in a selectivity shift from ethylene to methane while maintaining low hydrogen evolution activity.

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Highlights

Tuning the CO_2 reduction reaction product distribution by disrupting C-C coupling

Porous Ga-doped CuAl catalysts were synthesized

Methane current density of 234 mA/cm^2 and faradaic efficiency of 53% were achieved

Stable operation over 10 h



Article

Ga doping disrupts C-C coupling and promotes methane electroproduction on CuAl catalysts

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SUMMARY

The electrochemical CO₂ reduction reaction (CO₂RR) provides a route to store intermittent electricity in the form of fuels like methane. We reasoned that disrupting C-C coupling while maintaining high *CO coverage could enhance methane selectivity and suppress the hydrogen evolution reaction (HER). We studied the effect of doping CuAl, a material at the top of the CO₂RR activity and selectivity volcano plot, with elements having low *CO binding energies: Au, Zn, and Ga. Encouraged by initial improvements in selectivity to methane, we optimized the Ga content and showed that the presence of uniformly dispersed Ga is crucial in CO₂RR-to-methane performance enhancement. We rule out porosity and roughness and conclude that the presence of Ga in the doped catalysts enables high methane selectivity. The Ga-doped CuAl catalysts achieve a methane Faradaic efficiency (FE) of 53% by suppressing HER to 23% in neutral electrolyte at -1.4 V versus reversible hydrogen electrode.

INTRODUCTION

Toward the goal of storing intermittent, seasonably variable, renewable electricity, it is of potential interest to explore and advance the electrochemical production of methane, a commodity for which the infrastructure for transportation, storage, and use is well developed.^{1,2}

Previous works used different strategies to boost the methane selectivity, such as Cu⁽⁰⁾-based catalysts,³ doping Cu structures with metal oxides clusters,^{4,5} tuning the CO₂ partial pressure,^{6,7} low-coordination-number Cu clusters,⁸ and metal-free C-based catalysts.⁹ However, Cu alloying and doping elements into Cu-based structure have yet to contribute to selective CO₂RR-to-methane performance of Cu at industrially relevant production rates. Cu is selective toward hydrocarbons,^{10,11} and doping different elements—particularly d-block, group 3A, and 4A elements^{6,12–18}—into Cu offers avenues to improve CO₂RR selectivity toward a specific product via tuning the reaction intermediate binding energies, and thus, product distributions are affected by the chemical composition and available binding sites of the catalyst.¹⁹ Synthesis methods to achieve these doped Cu materials, such as co-sputtering,^{13,20} co-electrodeposition,¹² and galvanic exchange,^{18,21} result in different product distributions.

In the present work, we sought a Cu-based methane-selective catalyst to simultaneously suppress the hydrogen evolution reaction (HER) and C₂₊ production. Prior works have indicated a trade-off in electrocatalyst design for methane: lowering the CO₂ partial pressure leads to lower *CO coverage and suppresses C-C coupling,^{6,7} thus benefiting C₁ production, mainly methane, but at the expense of

The bigger picture

The energy grid needs to shift from fossil fuels to renewable energies, such as wind, solar, nuclear, and hydroelectric energy, in order for society to keep below the 1.5°C global warming threshold. One challenge in achieving this goal is the intermittency of wind and solar electricity. An approach is the electrically powered production of methane, a commodity for which the infrastructure for storage, transportation, and use is well developed. CO₂RR-to-methane catalysts are in need of improved selectivity, productivity, and stability. Herein, we show how the CO₂RR product distribution can be redirected from C₂₊ products to methane by disrupting carbon-carbon coupling. The material design principles herein contribute to the roadmap for CO₂RR electrocatalyst design.

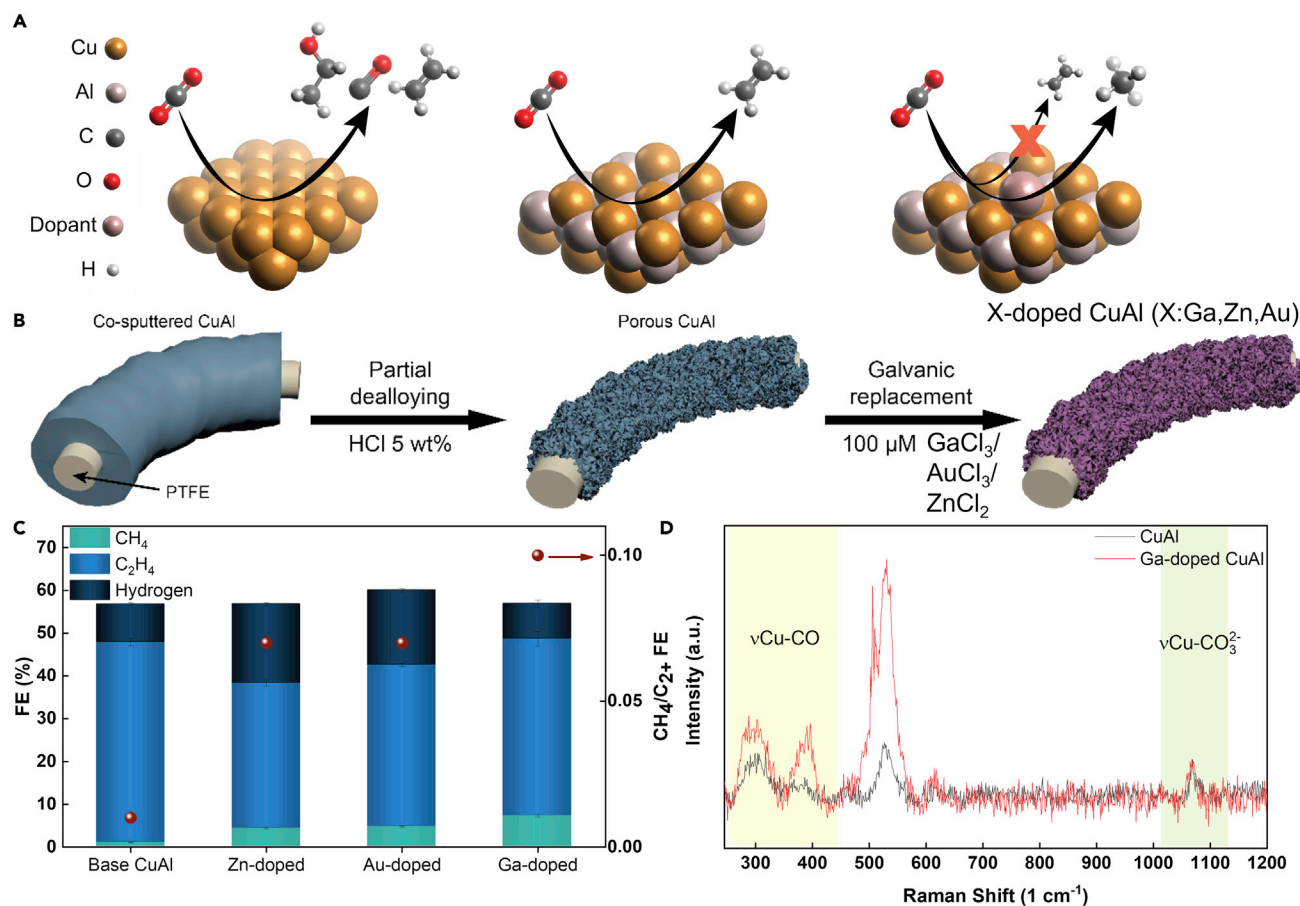


Figure 1. Proposed mechanism and material design principle for C-C disruption

(A) Dopant addition blocks C-C coupling and shifts the product distribution toward methane.

(B) Three-step synthesis method of doped CuAl catalysts.

(C) Gas product FE of CuAl and doped CuAl catalysts with different dopants in 1 M KOH at -1.5 V versus RHE ($n = 3$ replicates).

(D) Comparison of *in situ* Raman spectra of 8-min Ga-doped CuAl and CuAl catalyst in 1 M KHCO₃ with a current density of 25 mA cm^{-2} (-0.9 V versus RHE). The region of $280\text{--}430 \text{ cm}^{-1}$ showing Cu-CO stretch is shaded.

high HER. Local pH on the catalyst surface affects the CO₂RR product distribution since *CO protonation is a pH-dependent step.^{22–25} C-C coupling is disrupted at lower pH, leading to higher selectivity toward methane; however, HER also increases in lower pH.

We pursued therefore a strategy to disrupt C-C coupling in the regime of high *CO coverage since the high *CO coverage can be levered to suppress HER (Figure 1A).^{26,27}

We began from a starting point of CuAl binary catalysts since these feature near-ideal *CO binding energies.²⁰ We posited that adding an element with low *CO binding energies to CuAl catalysts could disrupt C-C coupling.^{28,29} We doped base CuAl with Zn, Au, and Ga, which have low *CO binding energies,^{29–32} and observed a product distribution shift from C₂₊ products to methane in each case. We optimized Ga-doped CuAl catalysts and reached 53% FE to methane. We studied the optimized Ga-doped CuAl catalysts, which are both porous and rough, and found the improvement in underlying methane activity is from the Ga doping and not due to change in porosity and roughness. *Operando* Raman spectroscopy

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revealed that the introduction of Ga into CuAl tends to increase *CO coverage, resulting in a lower HER. The shift in the product distribution from C_{2+} to methane on Ga-doped CuAl catalysts while maintaining a high *CO coverage indicates that the desired *CO protonation step is promoted compared with the C-C coupling step. We studied Ga-doped CuAl catalysts under -1.4 V versus reversible hydrogen electrode (RHE) and found that these maintained an FE above 45% for over 10 h.

RESULTS AND DISCUSSION

To explore the CO_2RR performance of X-doped (X: Au, Zn, or Ga) CuAl, we synthesized porous catalysts via a three-step method (Figure 1B). Cu and Al are first co-sputtered onto a polytetrafluoroethylene (PTFE) gas diffusion layer (GDL) with a thickness of 200 nm (Figure S1), resulting in a layered hydrophilic/hydrophobic structure—an approach known to enhance the transport of gaseous species.²² The CuAl layer is then partially dealloyed in 5 wt % HCl solution for T min (4–8 min). Finally, X is added by immersing the CuAl in X chloride solution, leading to the galvanic replacement of Al in the porous CuAl with X. When we attempted extended dealloying exceeding 8 min following galvanic exchange for more than 2 h, we found delamination of the catalyst layer from the PTFE GDL, which we attribute to accelerated corrosion (Figure S2).

We carried out CO_2RR in a flow cell reactor using an alkaline electrolyte (1 M KOH). Compared with CuAl, the series of X-doped 6-min CuAl catalysts (dealloyed for 6 min and doped via galvanic exchange process for 2 h) showed higher methane FE and methane/ C_{2+} FE ratio (Figure 1C). We chose Ga-doped CuAl catalysts to investigate the reason behind the methane selectivity increase compared with CuAl through *operando* Raman (Figure 1D).³³ The similar Cu- CO_3^{2-} stretch intensities in base CuAl and Ga-doped CuAl Raman spectra ($1,040$ – $1,100$ cm^{-1}) indicate a similar surface-enhanced Raman spectroscopy (SERS) effect in Ga-doped CuAl and CuAl. Although Ga-doped CuAl shows higher methane selectivity than CuAl, we found a higher *CO coverage (280 – 430 cm^{-1}) on the Ga-doped CuAl surface than CuAl. The higher *CO coverage on Ga-doped CuAl may be attributed to *CO intermediate formation on Ga and then the transfer of that to CuAl surface.^{17,34} However, we observed a high methane selectivity under high *CO coverage, leading to HER suppression, indicating that Ga addition into CuAl tends to disrupt C-C coupling and facilitate *CO protonation instead. Previous studies have shown the C_{2+} product selectivity generally increases with increasing *CO coverage;^{7,35,36} however, at very high *CO coverages, the reaction barrier, enthalpy change of *CO dimerization,³⁵ and *H binding energies all increase,³⁷ steering the selectivity away from HER and C_{2+} products. The uniform distribution of Ga increases under-coordinated Cu (Figure S3), leading to stronger *CO binding energies on the Cu surface and preventing its further movement for C-C coupling.^{8,34}

We also note that the Ga distribution is more uniform (viz. energy-dispersive X-ray spectroscopy [EDX] mapping; Figures 2A, S4, and S5) in Ga-doped CuAl catalysts compared with Zn and Au distribution in Zn-doped and Au-doped CuAl catalysts. Galvanic replacement occurs between Ga^{3+} and $Al^{(0)}$ on the CuAl surface, since Ga has a standard reduction potential (-0.53 V versus standard hydrogen electrode [SHE]) between Al (-1.66 V versus SHE) and Cu (0.34 V versus SHE).³⁸ Previous studies on doping Cu-based materials via galvanic exchange have shown that the doping penetration depth is typically limited to 50–100 nm, which is directly correlated with the galvanic exchange kinetics.^{39–41} The differences between the standard reduction potentials of the dopants versus Al are higher in the cases of Zn-doped and Au-doped CuAl catalysts compared with that in Ga-doped CuAl

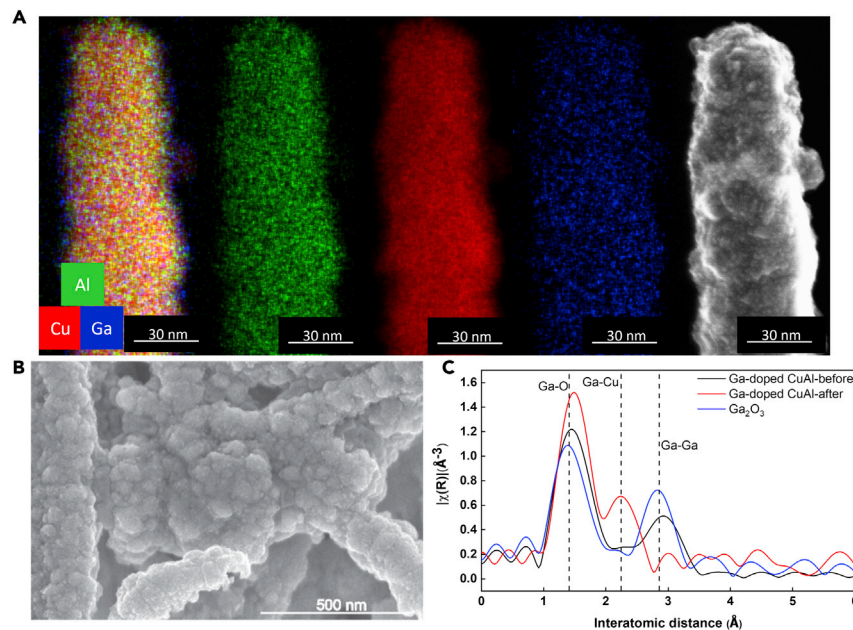


Figure 2. Characterization of Ga-doped CuAl catalysts

(A) EDX mapping and a high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) image of Ga-doped 8-min CuAl catalyst.

(B) Scanning electron microscopy image of a representative Ga-doped 8-min CuAl catalyst.

(C) Ga K-edge extended X-ray absorption fine structure (EXAFS) for Ga-doped 8-min CuAl catalyst before and after CO₂RR and reference Ga₂O₃.

catalysts. This accounts for a less uniform distribution of Au and Zn on the CuAl surface than Ga distribution on the CuAl surface (Figure S5).^{38,39} We observed high porosity for all the doped CuAl catalysts (Figures 2B and S5). We attribute the low methane selectivity of Au-doped CuAl compared with previously reported CuAu to the difference in inlet CO₂ partial pressure and a non-uniform distribution of Au on CuAl translating into Au agglomeration and large Au-particle formation on the CuAl surface (Figure S5).⁶ Higher *H binding energies on the isolated Au surface on Au-doped CuAl compared with Zn- and Ga-doped CuAl surfaces account for increased HER on Au-doped CuAl.^{6,42}

To investigate the structure of Ga-doped CuAl under CO₂RR, we performed *ex situ* Ga K-edge X-ray absorption spectroscopy (XAS) and X-ray diffraction (XRD) (Figures 2C, S6, and S7). Before CO₂RR, Ga is present as an oxide (Ga₂O₃), whereas, following CO₂RR, the Ga-Cu peak intensity increases and the Ga-Ga peak decreases. We conclude that the interaction between Cu and Ga increases after CO₂RR, consistent with Ga being dispersed more uniformly (Figure 2C). *Ex situ* Ga K-edge X-ray absorption near-edge structure (XANES) reveals that the white line height increases after CO₂RR (Figure S6): this we attributed to the hybridization of Ga 4p orbitals with those in Cu, increasing empty 4p orbitals, consistent with the view that Ga diffuses in the CuAl structure and forms CuGa alloys. Taking together knowledge of the local pH during CO₂RR, the Ga Pourbaix diagram, and XAS results, we conclude that Ga is in the Ga₂O₃ state before reaction and is part of a Ga-Cu alloy in electroreduction (Figures S7 and S8).

We further optimized the Ga-doped CuAl structure by tuning Ga concentration systematically and studying CO₂RR performance in an alkaline electrolyte (1 M KOH; Figures 3

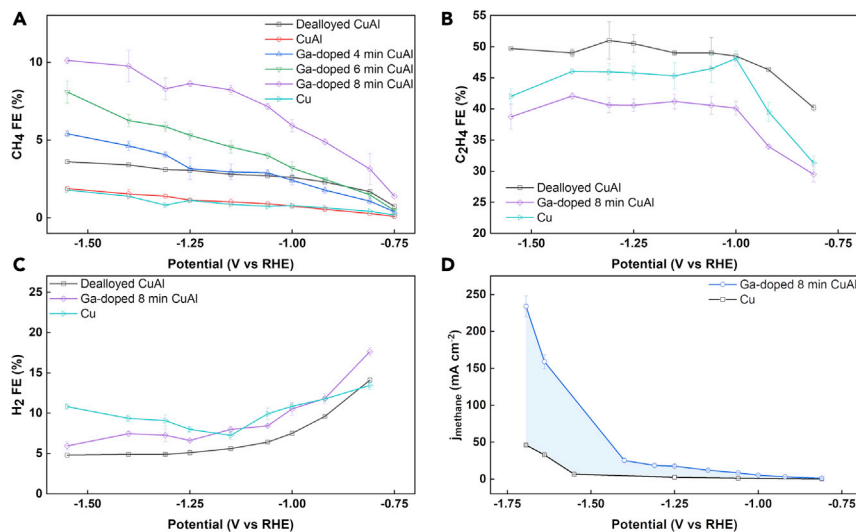


Figure 3. Product distribution of Cu, CuAl, and Ga-doped CuAl catalysts with 1 M KOH electrolyte

(A–C) Methane FE versus potential (A), ethylene FE versus potential (B), and hydrogen FE versus potential (C).

(D) Methane partial current density versus potential ($n = 3$ independent replicates).

and S9). Methane selectivity increases with dealloying duration (Figure S10). Ga-doped catalysts with Ga concentrations higher than 7.2 wt % show a decrease in both methane and ethylene selectivity: indeed, too much Ga may interfere with Cu active sites. Prior reports reveal that overly high Ga concentration permits the desorption of *CO and may prevent the *CO protonation step needed in methane formation (Figures 2A and S10A), also in agreement with Cu-based binary catalyst studies in which the dopant has a low CO binding energy.^{6,13} A computational study predicted that *CO binding energies decrease on CuGa intermetallic catalysts with increasing Ga concentration.³⁰

We propose that the addition of Ga to CuAl shifts the product distribution from C₂₊ products to methane by disrupting C-C coupling. We sought to verify the hypothesis, testing the effect of catalyst layer roughness and porosity on performance (Figures S11 and S12; Table S1). We performed CO₂RR experiments on porous Cu: methane FE decreased with increasing porosity, as seen in previous reports.²⁰ In contrast, the FE on Ga-doped CuAl samples increased with dealloying time, and the roughness of the Ga-doped CuAl samples are very similar, thus linking the increase in methane FE to the addition of Ga, despite the increased surface roughness and porosity that accompanies it.

We found that Ga-doped CuAl catalysts show lower ethylene and C₂₊ product FEs than Cu and dealloyed CuAl catalysts (Figure 3B; Table S2). We observed a lower hydrogen FE on Ga-doped CuAl and dealloyed CuAl than Cu (Figure 3C), hinting at a higher *CO coverage on them that suppresses HER. Ga-doped CuAl catalysts show a higher methane partial current density than Cu, i.e., higher activity (Figure 3D). We obtained a high methane partial current density of 234 mA cm⁻² at -1.7 V versus RHE with a methane FE of 30% in an alkaline electrolyte with the Ga-doped 8-min CuAl (referred to as Ga-doped CuAl from here onward; Figures 3D and S9D).

To improve further the system-level CO₂RR-to-methane performance, we changed to a neutral pH electrolyte, seeking lower CO₂ crossover^{43,44} and also increased

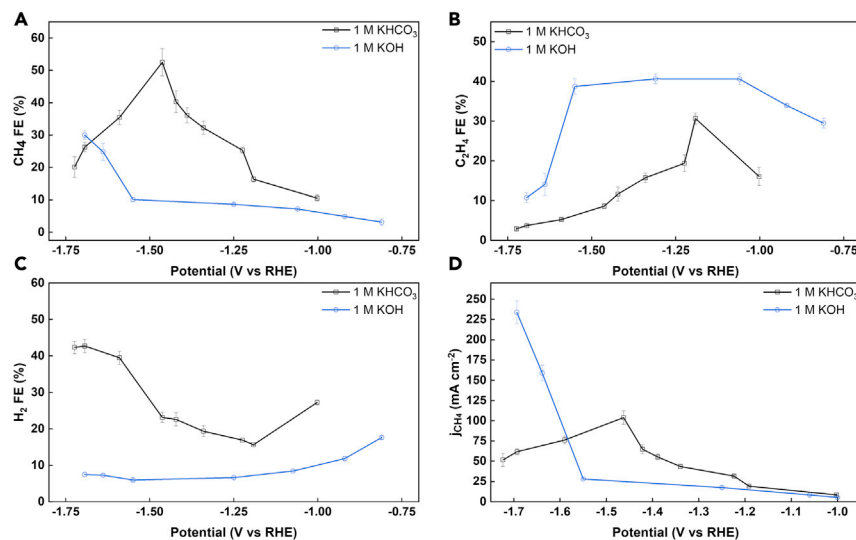


Figure 4. Ga-doped 8-min CuAl CO₂RR performance in a neutral electrolyte (1 M KHCO₃) compared with alkaline electrolyte (1 M KOH)

(A–C) Methane FE versus potential (A), ethylene FE versus potential (B), and hydrogen FE versus potential (C).

(D) Methane partial current density comparison between neutral electrolyte (1 M KHCO₃) and alkaline electrolyte (1 M KOH) on Ga-doped 8-min CuAl catalysts under different applied potentials (n = 3 independent replicates).

*CO protonation.⁴⁵ In 1 M KHCO₃ electrolyte, we obtained a methane FE of 53% at –1.4 V versus RHE with a methane partial current density of 109 mA cm⁻², accompanied by decreased ethylene FE (Figure 4B). Previous studies have shown that Ga is a CO₂RR-to-CO catalyst, consistent with a low *CO binding energy:^{28,29} one possibility is that *CO coverage on non-Ga sites may increase due to the spillover of *CO from Ga to the non-Ga active sites, a phenomenon observed in other Cu-based catalysts containing CO-selective metals.^{17,36} We observed a higher methane partial current density in neutral pH electrolyte (1 M KHCO₃) with potentials more positive than –1.4 V versus RHE compared with that in an alkaline electrolyte (Figure 4D).

We studied the Ga-doped CuAl catalyst structure following 11 h of operation under CO₂RR at constant potential –1.4 V versus RHE in 1 M KHCO₃ (Figure 5). Catalysts showed stable CO₂-to-methane electrolysis for over 10 h, maintaining methane FE above 45% (Figure 5A). We observed no change in the bulk electrolyte pH showing no CO₂ and OH⁻ loss in the electrolyte, unlike alkaline electrolytes.⁴⁶ We characterized the morphology and chemical composition of the catalyst before and after CO₂RR (Figures 5B and 5C). Scanning electron microscopy (SEM) images showed no appreciable changes to surface morphology.

In sum, this work reports Cu-based ternary catalyst materials (doped CuAl) for methane production via CO₂RR. We explored synthesis parameters and achieved a methane FE of 30% in an alkaline electrolyte (1 M KOH) with Ga-doped CuAl catalysts. We further improved the methane FE of Ga-doped CuAl by moving to a neutral electrolyte (1 M KHCO₃) and obtained a methane FE of 53% at a methane partial current density of 109 mA cm⁻² and –1.4 V versus RHE (Table S3). We studied the origins of improved performance in Ga-doped CuAl with *operando* Raman spectroscopy, as well as roughness and porosity control studies. The findings support the

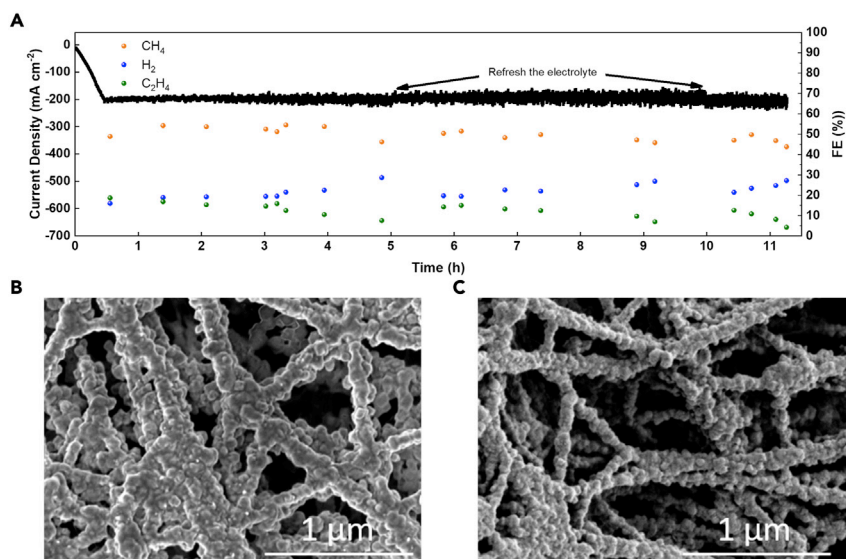


Figure 5. Stability measurements and pre- and post-operation characterization

(A) Ga-doped 8-min CuAl catalyst product distribution under CO₂RR with 1 M KHCO₃ as the electrolyte and a constant potential of -1.4 V versus RHE over time (the applied potential was gradually decreased to -1.4 V versus RHE over the first 30 min).

(B and C) SEM images before (B) and after (C) the long-term stability test. The post-CO₂RR characterizations were done on Ga-doped 8-min CuAl after performing CO₂RR for 10 h under -1.4 V versus RHE in 1 M KHCO₃.

view that C-C coupling is disrupted by Ga, leading to a product distribution shift from C₂₊ products, including ethylene to methane. We assessed the stability of the Ga-doped CuAl catalyst and observed that the catalyst structure is unchanged during CO₂RR.

EXPERIMENTAL PROCEDURES

An extensive description of materials, sample fabrication, and characterization can be found in [supplemental information](#).

Resource availability

Lead contact

Further information and requests for resources should be directed to and will be fulfilled by the lead contact, Edward H. Sargent (ted.sargent@utoronto.ca).

Materials availability

This study did not generate new unique reagents. Any materials used are available from the [lead contact](#).

Data and code availability

Data are available upon request from the [lead contact](#). No code was generated. Full experimental procedures are provided in the [supplemental information](#).

SUPPLEMENTAL INFORMATION

Supplemental information can be found online at <https://doi.org/10.1016/j.cheecat.2022.03.016>.

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AUTHOR CONTRIBUTIONS

E.H.S. supervised the project. A.S.R. conceived the idea and designed and carried out the experiments. J.W. and K.B. carried out the XPS. S.-F.H., F.-Y.W., and J.A. conducted and analyzed XAS experiments. J.E.H. contributed to the characterization of the materials. X.W., J.W., and C.-T.D. contributed to the discussion and results. All authors discussed the results and assisted during manuscript preparation.

DECLARATION OF INTERESTS

The authors declare no competing interests.

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